





Detailed Energy Audit Report

M/s Rajasthan Tools Nagaur Handtools Cluster

Under GEF-UNIDO-BEE project

Promoting energy efficiency and renewable energy in selected MSME clusters in India

January 2016



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List of abbreviations

APFC Automatic Power Factor Controller AVVNL Ajmer Vidyut Vitran Nigam Limited

BEE Bureau of Energy Efficiency

DISCOM Distribution Company

GEF Global Environment Facility

HP Horsepower kCal Kilo Calories kVA Kilo Volt Ampere

kVAr Kilo Volt Ampere reactive

kW Kilo Watt kWh Kilo Watt Hour

MSME Micro, Small and Medium Enterprises

MT Metric Tonne

PMU Project Management Unit

UNIDO United Nations Industrial Development Organization

Acknowledgement

We sincerely thank GEF- UNIDO-BEE for associating PricewaterhouseCoopers Private Limited (PwC) in its prestigious project "Promoting energy efficiency and renewable energy in selected MSME clusters in India" which involves developing and promoting market environment for introducing energy efficiencies in process applications in 12 selected energy-intensive MSME clusters in India. Nagaur handtools cluster is one of them.

We express our sincere gratitude to all following officials of GEF-UNIDO-BEE PMU for their valuable support and guidance during the project:-

- Mr. Milind Deore, Energy Economist, BEE
- Mr. Abhishek Nath, National Project Manager, UNIDO
- Mr. Niranjan Rao Deevela, National Technology Coordinator, UNIDO
- Mr. Ashish Sharma, Project Engineer, BEE

PwC is thankful to Nagaur Handtool Manufacturer's Association for extending support for this assignment. We are also thankful to Mrs. Mumtaz Begum, Owner, Rajasthan Tools and his team for giving full support during the energy audit. We would like to thank Mr. Rajiv Singhal, Cluster Leader, GEF-UNIDO-BEE Project for providing on-field support during the energy audit.

Executive Summary

Rajasthan Tools is located in Basni Industrial Area of Nagaur and is involved in manufacturing of pliers. It uses EN 8 as raw material which is sheared into appropriate size through a shearing machine. Thereafter, blanks are fed to reheating furnace for heating up to a temperature of around 1150 - 1200 °C. After which the heated blank is rolled and pressed to give the shape of plier. During the process, excess material is cut and finally end cutting is done so that the final product is of correct size.

During the energy audit, following energy efficiency opportunities were identified:

S.No.	Energy Efficiency measure	Investment (INR)	Savings (INR)	Payback period (months)
1	Installation of Automatic Power Factor Controller (APFC)	23,625	11,150	25
2	Installation of electric billet heater	11,27,000	3,76,385	36
3	Installation of cogged belt on load side and poly-V belt on common shaft drive side	12,723	9,450	16
4	Preheating arrangement for raw material	20,000	76,388	3
	Total	11,83,348	4,73,373	30

The details about the unit, load profiles, efficiency of furnace and description of energy conservation measures are discussed in appropriate sections of the report.

Project Background

1.1. Background of the project

GEF-UNIDO-BEE is developing and promoting market environment for introducing energy efficiencies in process applications in 12 selected energy-intensive MSME clusters in India which includes Nagaur handtools cluster also.

The overall motive of this assignment is to improve the productivity and competitiveness of units as well as to reduce overall carbon emissions and improve the local environment.

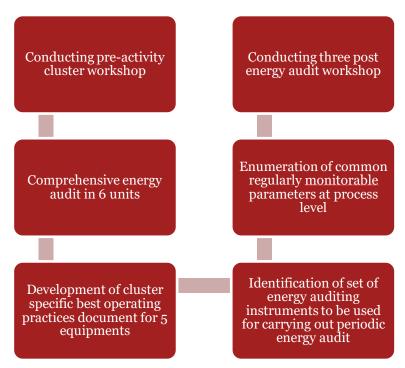
1.2. Introduction to assignment

Under GEF-UNIDO-BEE project 'Promoting energy efficiency and renewable energy in selected MSME clusters in India', PwC has been appointed for conducting activities of energy audit and dissemination in the Nagaur Handtools Cluster.

1.3. Scope of services

The activities being conducted by PwC under this assignment are shown at **Error! Not a valid bookmark self-reference.**.

Figure 1: Scope of services



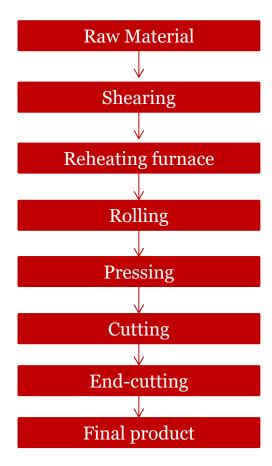
This current report has been prepared under the task 2 of above scope of services i.e. conducting comprehensive energy audits in 6 units in the cluster.

2. Energy Audit at Rajasthan Tools

2.1. Process flow

The process flow at Rajasthan Tools is shown at Figure 2 below. The raw material (EN 8) is sheared into appropriate size through a shearing machine. Thereafter, blanks are fed to reheating furnace for heating up to a temperature of around 1150 - 1200 °C. After which the heated blank is rolled and pressed to give the shape of plier. During the process, excess material is cut and finally end cutting is done so that the final product is of correct size. This is depicted in the following figure.

Figure 2: Process flow



The specialized instruments that were used during the energy audit included:

- Non-contact Infrared Thermometer (Testo-845 and Extech)
- Flue Gas Analyzer (KANE 900+)
- 3-phase Power Analyzer (Krykard ALM 30)
- 1-phase Power Analyzer (Krykard ALM 10)
- Vane Anemometer (Testo-416)
- Digital Tachometer (Extech-461995)

Details about the make of energy audit instruments are provided at **Annexure A.**

This report presents the field measurements, design and operational data and data analysis.

2.2. Baseline information of Rajasthan Tools

In order to assess the present energy consumption levels and possible energy efficiency measures at 'Rajasthan Tools' basic and general information was collected during the audit conducted on 4th and 5th May 2015.

The detail of energy audit of unit is provided below.

2.2.1. About the Unit

This unit is located in Basni Industrial Area of Nagaur. The baseline profile of the unit is presented in Table 1.

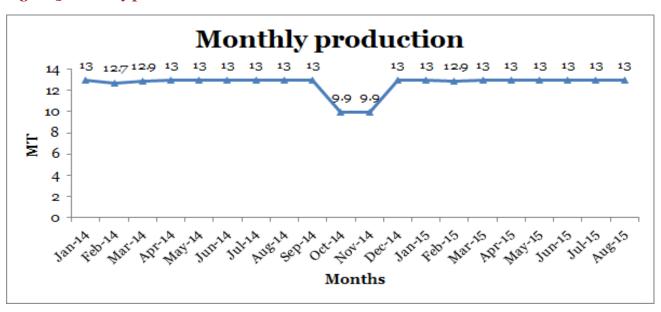
Table 1: Baseline profile

Parameters	Details
Name of the unit	Rajasthan Tools
Name & contact number of contact person	Mrs. Mumtaz Begum Mobile - 9887786911
Date of audit	4th and 5th May 2015
Raw material	EN-8
Final product	Plier 6"
Furnace	Box type
Dimension of furnace	33" X 19" X 16"
Fuel used	Furnace oil
Press hammer weight	150 kg
Daily production	1300 pieces
Operating hours/day	7 hours
Sanction load	40 hp

2.3. Monthly trend of production

The audit team has collected monthly production data from the unit and the same has been depicted in the following figure.

Figure 3: Monthly production data



2.4. Past electricity bill analysis

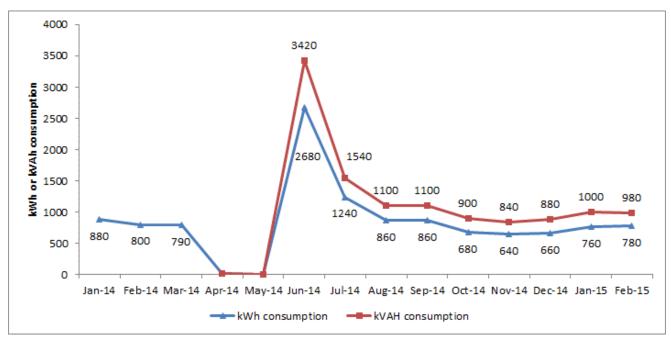
The team has collected electricity bills from January 2014 to February 2015 for the purpose of analysis. The electricity bills from January 2014 to March 2014 were based on LT-5 category as specified by AVVNL with sanction load of 15 hp. However, from April 2014 onwards, the tariff category was changed to LT-6 due to increase in sanction load to 40 hp. The details of these tariff categories are tabulated below:

Table 2: Tariff description

Parameter	LT-5	LT-6
Category description	Sanction load above 5kW but not	Sanction load above 25 HP but
	exceeding 25HP	not exceeding 150 HP
Fixed charges	INR 50/ kVA	INR 60/ kVA
Energy charges	INR 4.85/ kWh	INR 6.25/ kWh

A graph showing pattern of energy consumption is shown below.

Figure 4: Energy consumption pattern



It can be inferred from above figure that the energy consumption peaks during months of June, January and February after which the consumption decreases. Further, the average energy consumption, for the said period, is 969 kWh/month.

Similarly, the power factor profile as well as power factor surcharge paid by the unit are shown in following figure.

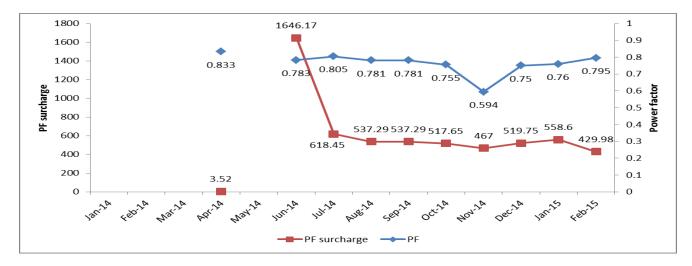


Figure 5: Power factor profile and power factor surcharge

It can be seen that the unit has paid around INR 5900 due to low power factor surcharge from January 2014 to February 2015.

2.5. Load profile of Rajasthan Tools

In order to derive the load profile of the unit, many electrical parameters were measured by using a sophisticated portable 3-phase power analyser (KRYKARD).

2.5.1. Load (kW) and apparent power (kVA) profile

Load profile and apparent power profile is a graph of the variation in the electrical load versus time. In any electrical system, the vector sum of the active power (kW) and reactive power (kVAr) make up the total (or apparent) power (kVA) used. This is the power generated by a generation station for the user to perform a given amount of work. Total power is measured in kVA (Kilo Volts-Amperes) and the load or active power is measured in kW (kilowatts) and they become equal as and when the power factor approaches unity. Total electricity charges (units and demand) are based on the load or active power (kW) and apparent power (kVA).

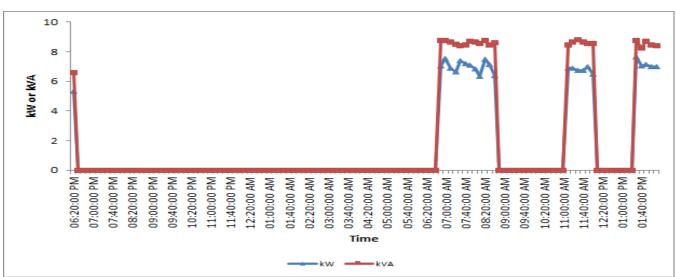


Figure 6: Active power (Load) and apparent power profile during audit

Observations made from the above graph:

• The maximum input power drawn by the unit is 7.63 kW. The graph shows that that the unit stopped operation around 6:30 PM and then began its operation from 6:20 AM onwards.

Apparent power curve (kVA) line is significantly above the active power (kW) line indicating that power factor is on lower side.

2.5.2. Electricity consumption (kWh) profile

Electricity consumption profile is the pattern of the consumption of electricity in the unit during the energy audit. The following graph captures the electricity consumption (kWh) profile of the unit:

40 35 30 20 15 10 5 o 09:40:00 PM 09:40:00 AM 01:00:00 PM D7:00:00 PM 07:40:00 PM 38:20:00 PM M9:00:00:00 .0:20:00 PM 11:00:00 PM 1:40:00 PM 2:20:00 AM 11:00:00 AM 11:40:00 AM 02:20:00 AM 03:00:00 AM 03:40:00 AM 04:20:00 AM 05:00:00 AM 05:40:00 AM 06:20:00 AM 7:00:00 AM 7:40:00 AM 8:20:00 AM 9:00:00 AM 1:00:00 AM 1:40:00 AM Energy (kWh) Energy (kVAh)

Figure 7: Electricity consumption (kWh) and (kVAh) profile during audit

Observations made from the above graph:

The unit consumed nearly 27.69 kWh and around 34.02 kVAh during the recording period of almost 19 hours.

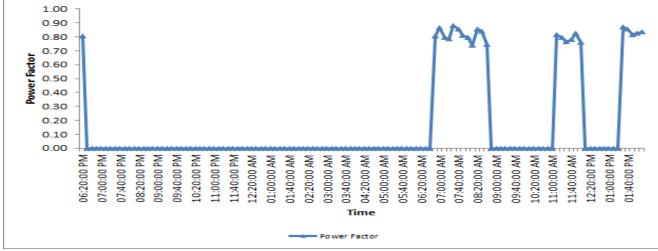
2.5.3. Power factor profile of the unit

Power factor is an important parameter for the unit since its billing is based on kVAh wherein power factor plays a major role. Also, DISCOM's supplying power to the units impose power factor surcharge on the bills in case the power factor is below 0.90.

The following graph captures the power factor profile of the unit:



Figure 8: Power factor profile during audit

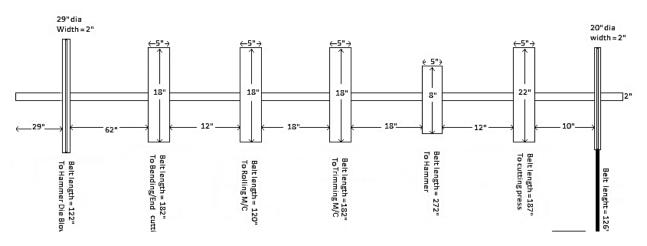


Observations made from the above graph:

- The power factor of the unit is on lower side with maximum power factor being at 0.88
- The unit may consider installing capacitor banks for improving the power factor so that they do not get charged with power factor surcharge.

A common shaft is used in the unit for transmission of power from drive motor to other loads. The layout and positioning of various loads and centre distances are depicted in following figure.

Figure 9: Different loads and centre distances of pulleys on common shaft

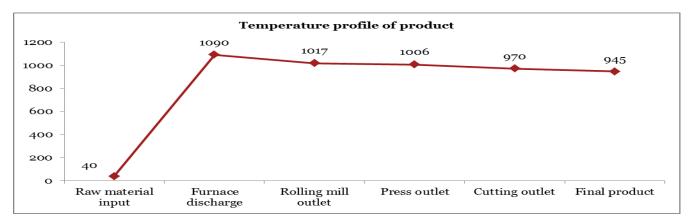


2.6. Temperature profile of process and furnace

2.6.1.1. Temperature profile

During the baseline energy audit, temperature was measured at various stages of the process such as raw material temperature, furnace discharge, rolling mill outlet, press outlet, cutting outlet and final product. The temperature profile is presented at following figure.

Figure 10: Temperature profile from raw material to final product



There is total temperature drop of around 145°C from furnace outlet till final product.

2.6.1.2. Skin temperature

The skin temperature of furnace was captured using infrared thermometer. The temperature profile is mentioned below:

Figure 11: Skin temperature of furnace

Dis	scharge s	ide	Back	Side
286	300	315	250	238
206	270	300	203	160
	280		2 1	L3
В	urner sid	le		
266	250	235		
253	232	180		
	236			

It can be observed that the skin temperature is very high indicating that refractory lining is not proper inside the furnace and it also indicates that surface insulation is not present.

2.7. Thermal efficiency of furnace - direct method

Furnace thermal efficiency calculation by direct method involves comparison of useful heat content in the stock with the total thermal energy input to the furnace. Thermal efficiency for the reheating furnace is calculated by direct method in table below.

Table 3: Thermal efficiency of furnace - direct method

Parameter	Unit	Value
Production on audit day	kg/day	629.20
Furnace throughput	kg/hr	89.89
Fuel consumption rate	kg/hr	9.39
Gross calorific value of fuel	kCal/kg	10,880.00
Specific heat of the material	kCal/kg °C	0.12
Material charging temperature	°C	40.00
Material discharge temperature	°C	1,090.00
Furnace efficiency by direct method	%	11.08

It can be seen from above table that furnace thermal efficiency is around 11% as calculated by direct method. However, using direct method, one cannot determine different heat losses associated with furnace operation. Hence, indirect method or heat loss method is employed to determine furnace thermal efficiency as well as heat losses due to various other factors. The same has been discussed in next.

2.8. Thermal efficiency of furnace - indirect method

Indirect Method helps to determine major heat loss from furnace which includes losses in flue gas and other heat loss parameters like surface radiation losses, CO formation loss, etc. All these losses are calculated in table below:

Table 4: Thermal efficiency of furnace - indirect method

Parameter	Unit	Value
Measured O ₂ in flue gas	%	6.10
Measured CO in flue gas	ppm	9225
Excess air used for combustion	%	40.94
Corresponding CO ₂	%	12.37
Total air used for combustion	kg/kg of fuel	18.20
Sensible heat loss in flue gas	%	60.35
Heat loss due to moisture present in fuel	%	0.019
Heat loss due to evaporation of water formed due to hydrogen in fuel	%	7.24
Heat loss due to moisture present in air	%	1.67
Heat loss due to CO formation	%	3.23
Heat loss due to radiation and openings	%	5.49
Heat loss in scale generation	%	0.003
Heat content in the material	%	11.08
Unaccounted Heat Losses	%	10.92

The exit flue gas temperature of furnace is 1050 °C and it can be observed from above that heat loss due to flue gas is one of the major contributors to overall heat loss from the furnace followed by heat loss due to hydrogen in fuel and heat loss due to radiation & openings. Detailed calculation sheet is attached at Annexure B.

2.9. Material loss during production

As observed in the process flow, material loss happens in following forms:

- Burning loss
- · Cuttings after pressing
- · End cuttings after sizing of product

We have captured these parameters to assess the burning loss as well as other material loss during the production process.

The assessment is tabulated below:

Table 5: Material loss during production

Parameter	Unit	Value
Weight of raw material	kg/piece	0.242
Weight of final product	kg/piece	0.204

Weight of cuttings	kg/piece	0.025
Weight of end-cuttings	kg/piece	0.006
Material loss in cuttings & end-cuttings	kg/piece	0.031
Total material loss	kg/piece	0.037
Burning loss	kg/piece	0.005
Burning loss	%	2.34%
Total material loss	%	15.39%

2.10. Specific energy consumption

Specific Energy Consumption for the product is calculated by aggregating individual specific energy consumption of fuel and electricity, as shown in table next.

Table 6: Specific energy consumption

Parameter	Unit	Value
Production	kg/day	629.20
Furnace oil consumption	L/day	71.48
Electricity consumption	kWh/day	26.80
Specific fuel consumption	L/Tonne	113.60
Specific electricity consumption	kWh/Tonne	42.60

3. Energy Conservation Measures

During the energy audit, we have identified following energy conservation measures:

- Installation of Automatic Power Factor Controller (APFC)
- Installation of electric billet heater
- Installation of cogged belt on load side and poly-V belt on common shaft drive side
- Preheating arrangement for raw material

We have analysed each of above mentioned measures next.

3.1. Measure 1: Installation of Automatic Power Factor Controller (APFC)

Recommendation

The average monthly power factor of the unit based on the electricity bills of the unit is 0.76 and it could be improved to 0.99 for load reduction and I²R losses reduction. This will also help in reducing the maximum demand. By installing Automatic Power Factor Control (APFC) unit, the power factor can be improved to unity.

Energy and financial savings

The following parameters and assumptions have been considered to estimate the energy savings and financial viability of this option:

Table 7: Power factor improvement - Assumptions and parameters considered for estimation of energy and financial savings

Assumptions and Input parameters				
Cost parameters				
Particulars	Unit	Value		
Tentative price of capacitor bank	INR/kVAr	900		
Tentative price of capacitor bank of 25 kVAr	INR	22,500		
Installation cost	% of capital cost	5		
Energy and financial s	savings			
Average monthly power factor		0.76		
Proposed power factor		0.99		
Required capacitor bank capacity	kVAr	25		
Total annual monetary savings through power factor incentives	INR	11,150		
Total investment requirement (price of capacitor bank and installation cost)	INR	23,625		
Simple payback period	Months	25		

The implementation of this recommendation will help the Rajasthan Tools to save around INR 11,150 per year by installing capacitor bank of around 25 kVAr. The implementation cost required to install Automatic Power Factor Control (APFC) panel is approximately INR 23,625 and the simple payback period of this investment is around 25 months.

3.2. Measure 2: Installation of electric billet heater

Recommendation

The efficiency of reheating furnace used in the unit is pretty low and it generates lot of smoke making the environment not suitable for the workers. So, we recommend installation of electric billet heater in place of existing furnace oil fired reheating furnace. This will result in higher efficiency of billet heater and also better working environment for the workers.

Energy and financial savings

The following parameters and assumptions have been considered to estimate the energy savings and financial viability of this option:

Table 8: Installation of electric billet heater - Assumptions and parameters considered for estimation of energy and financial savings

Assumptions and Input parameters				
Present Scenar	io			
Particulars	Unit	Value		
Existing burning loss	%	2.34		
Specific fuel consumption	L/T	113.6		
Hourly production	kg/h	89.89		
Present Scenar	io			
Size of billet heater	kW	40		
Proposed burning loss	%	0.35		
Specific electricity consumption	kWh/T	436		
Cost component	ts			
Cost of electric billet heater	INR	8,00,000		
Cost of new transformer	INR	1,50,000		
Miscellaneous expenses	INR	50,000		
Impact of increased sanction demand @ 40 kVA	INR	1,27,000		
Total cost	INR	11,27,000		
Electricity consumption	kWh/annum	82,303		
Electricity charges (in kWh/annum X INR 6.25/kWh)	INR	5,14,396		
Benefits				
Material savings	T/annum	3.76		
Fuel savings	L/annum	21,444		
Material savings (in T/annum X INR 43000/T)	INR	1,61,680		
Fuel savings (in L/annum X INR 34/L)	INR	7,29,101		
Total benefits (Material savings + Fuel savings - Electricity charges)	INR	3,76,385		
Simple payback period	Months	36		

The implementation of this recommendation will help the Rajasthan Tools to save around INR 3,76,385 per year by installing electric billet heater of around 40 kW capacity. This will not result in change in existing tariff category. The simple payback period of this investment is around 36 months.

3.3. Measure 3: Installation of cogged belt on load side and poly-V belt on common shaft drive side

Recommendation

Since the drive system in the unit is based on common shaft and different belts give input to other loads in the unit. Presently, the unit is using V-belt in common shaft drive side and flat belts on load side. However, if we replace existing belts with V-belt on load side and poly-V belt on common shaft drive side then it will give significant savings in electricity consumption of common drive motor as well as lower slippage losses.

Energy and financial savings

The following parameters and assumptions have been considered to estimate the energy savings and financial viability of this option:

Table 9: Installation of cogged belt on load side and poly-V belt on common shaft drive side - Assumptions and parameters considered for estimation of energy and financial savings

Assumptions and	d Input parameters	
	mptions	
Particulars	Unit	Value
Efficiency of V-belt	%	0.85
Efficiency of normal belt	%	0.8
Efficiency of poly V-belt	%	0.92
Efficiency of cogged belt	%	0.85
Hours of operation per day	Hours	7
Annual operation days	Days	300
Tariff	INR/kWh	6.25
	t Scenario	
kW consumed	kW	5.5
kW at drive shaft	kW	4.68
kW at load	kW	3.74
_	d scenario	
kW consumed	kW	4.78
kW at drive shaft	kW	4.40
kW at load	kW	3.74
Cost	elements	
Cost of 15 feet cogged belt type "C" (3 nos.)	INR	5386
Cost of 10 feet cogged belt type "C" (2 nos.)	INR	2404
Cost of 6 feet cogged belt type "C"	INR	595
Cost of 22 feet poly-V belt (2 nos.)	INR	2658
Installation of pulleys of appropriate size	INR	1680
Total cost	INR	12723
Ве	nefits	
Power savings	kW	0.72
Annual electricity savings	kWh/annum	1512
Monetary electricity savings	INR	9450
Simple payback period	Months	16

The implementation of this recommendation will help the Rajasthan Tools to save around INR 9450 per year by installing cogged and poly-V belts with an investment of INR 12723. The simple payback period of this investment is around 16 months.

3.4. Measure 4: Preheating arrangement for raw material

Recommendation

It was observed during the energy audit that exit flue gas temperature from furnace is as high as 1050 °C which is not being utilized. We have also observed that it takes approximately 90 minutes for processing a batch of 300 pieces. So, we propose installation of a preheating arrangement at exit of furnace wherein next batch of 300 pieces are kept. Thus, during that time next batch of 300 pieces can be preheated and then transferred into furnace for processing. This will result in significant savings in fuel without any changes in furnace efficiency.

Energy and financial savings

The following parameters and assumptions have been considered to estimate the energy savings and financial viability of this option:

Table 10: Installation of preheating arrangement for raw material - Assumptions and parameters considered for estimation of energy and financial savings

Assumptions and In	put parameters	
Assumpt		
Particulars	Unit	Value
Furnace efficiency	%	11.08
Material discharge temperature	°C	1090
Production	kg/h	89.89
Gross calorific value	kCal/kg	10880
Hours of operation per day	Hours	7
Annual operation days	Days	300
Fuel cost	INR/L	34
Present Sco	enario	
Material charging temperature	°C	40
Fuel consumption	L/day	71.49
Proposed sc	enario	
Material charging temperature	°C	150
Fuel consumption	L/day	64
Cost elem	ents	
Lump-sum cost for installation of preheating system	INR	20,000
Benefi	ts	
Fuel savings	L/day	7.49
Annual fuel savings	L/annum	2,246.72
Monetary savings due to fuel savings	INR	76,388
Simple payback period	Months	3

The implementation of this recommendation will help the Rajasthan Tools to save around INR 76,388 per year by installing preheating system for raw material with an investment of INR 20,000. The simple payback period of this investment is around 3 months.

Annexure A: List of Energy Audit Instruments

PwC has multiple energy audit instruments kits. All the instruments are of have high quality, precision and are periodically calibrated. The instruments are capable to cover all electrical and thermal measurements required in the plants. A list of instruments used by PwC during the audit are shown below:

S. No.	Name of the Instrument	Make	Quantity Used		
	Thermal Instruments				
1	Non-contact Infrared Thermometer (Testo-845 and Extech)	Testo (USA), Extech (USA)	2		
2	Flue Gas Analyzer (KANE 900+)	Kane (UK)	1		
	Electrical Instruments				
3	3-phase Power Analyzer	Krykard, Circutor and	3		
4	1-phase Power Analyzer	Extech	2		
Others					
5	Vane Anemometer (Testo-416)	Testo (USA)	2		
6	Digital Tachometer (Extech-461995)	Extech (USA)	1		

Annexure B: Calculation sheet of furnace efficiency by indirect method

Name of unit			D-1- 011
Name of unit No. of Energy Audit Product type Pilier Pilier	General Details		Data Sheet
No. of Energy Audit		Raiasthan Tools	
Product type			
Raw material under process			
Raw material under process	1 Todact type	i liei	
Production Capacity 0.6292 TPD Standard Temperature for operation 1090 °C Average scale loss 0.02342933 % Average plant operation 300 days/annum Tubel of tell Furnace Oil Type of fuel Furnace Oil Total carbon 88.9 % by mass Hydrogen content 0.5 % by mass Sulfur content 0.5 % by mass Oxygen content 1.4 % by mass Nitrogen content 0.5 % by mass Nitrogen content 0.5 % by mass Nitrogen content 0.5 % by mass Nitrogen content 0.35 % by mass Nitrogen content 0.5 % by mass Nitrogen content <td< td=""><td>Product size</td><td>160 mm</td><td></td></td<>	Product size	160 mm	
Standard Temperature for operation 1090 °C Average scale loss 0.02342933 % Average plant operation 7 hrs./day Fuel Details Type of fuel Furnace Oil Total carbon 88.9 % by mass Hydrogen content 8 % by mass Sulfur content 0.5 % by mass Oxygen content 1.4 % by mass Nitrogen content 0.5 % by mass Nitrogen content 0.5 % by mass Oxygen content 1.4 % by mass Nitrogen content 0.35 % by mass Oxygen content 0.35 % by mass Nitrogen content 0.35 % by mass Oxygen content 0.35 % by mass Nitrogen content 0.35 % by mass Oxygen content 0.35 % by mass Sulfur content 0.35 % by mass Coxtent 0.35 % by mass Ash content 0.35 % by mass Sel	Raw material under process	EN8	
Average plant operation 7 hrs./day Annual plant operation 300 days/annum Fuel Details Type of fuel Furnace Oil Total carbon 88.9 % by mass Hydrogen content 8 % why mass Sulfur content 0.5 % by mass Sulfur content 0.5 % by mass Nitrogen content 0.35 % by mass Nitro	Production Capacity	0.6292	TPD
Average plant operation	Standard Temperature for operation	1090	°C
Fuel Details Furnace Oil	Average scale loss	0.02342933	%
Type of fuel	Average plant operation	7	hrs./day
Type of fuel	Annual plant operation	300	days/annum
Total carbon	Fuel Details		
Hydrogen content	Type of fuel	Furnace Oil	
Sulfur content 0.5 % by mass Oxygen content 1.4 % by mass Nitrogen content 0.5 % by mass Moisture content 0.35 % by mass Ash content 0.35 % by mass Ash content 0.35 % by mass Gross calorific value 10880 kcal/kg. Bulk Density 920 kg/m³ Fuel consumption per hour 9.394514286 kg/hr Fuel consumption per day 65.7616 kg/day Fuel consumption per annum 19.72848 TPA Cost of fuel 31 Rs./kg Measured Data 8 C Measured Data 8 C Maberial Temperature : (DBT) 40 °C Ambient air temperature : (WBT) 38 °C Material Temperature at feeding 40 °C Temp. of supply air for combustion 40 °C Average Cypen level 6.1 % Average Cypel level 9225 ppm <t< td=""><td>Total carbon</td><td>88.9</td><td>% by mass</td></t<>	Total carbon	88.9	% by mass
Oxygen content Nitrogen content 0.5 % by mass Nitrogen content 0.35 % by mass Ash content 1080 kcal/kg, 1081	Hydrogen content	8	% by mass
Nitrogen content Moisture content O.35 Moisture content O.36 Moisture content O.37 Moisture content O.38 Moisture content O.39 Occupant Occu	Sulfur content	0.5	% by mass
Moisture content 0.35 % by mass Ash content 0.35 % by mass Gross calorific value 10880 kcal/kg. Bulk Density 920 kg/m³ Fuel consumption per hour 9.394514286 kg/hr Fuel consumption per day 65.7616 kg/day Fuel consumption per annum 19.72848 TPA Cost of fuel 31 Rs./kg Measured Data TPA Ss./kg Ambient air temperature: (WBT) 40 °C Ambient air temperature: (WBT) 38 °C Material Temperature at feeding 40 °C Temp. of supply air for combustion 40 °C Average Oxygen level 6.1 % Average poxygen level 6.1 % Average surface temperature -main body 200 °C Average surface temperature -main body 200 °C Average surface temperature -Top 200 °C Exit flue gas temperature at Discharge opening 1090 °C Tempera	Oxygen content	1.4	% by mass
Ash content Gross calorific value Bulk Density 920 kg/m³ Fuel consumption per hour 9.394514286 kg/hr Fuel consumption per day 65.7616 kg/day Fuel consumption per annum 19.72848 TPA Cost of fuel 31 Rs./kg Measured Data Ambient air temperature: (WBT) Ambient air temperature : (WBT) 38 °C Material Temperature at feeding 40 °C Temp. of supply air for combustion 40 °C Average Oxygen level Average CO level 9225 ppm Exit flue gas temperature - main body Average surface temperature - front & back Average Surface temperature - Top 1 Cande are a - main body 8 Cande are a - main body 9 Cande	Nitrogen content	0.5	% by mass
Gross calorific value 10880 kcal/kg.	Moisture content	0.35	% by mass
Bulk Density 920 kg/m³ Fuel consumption per hour 9.394514286 kg/m² Fuel consumption per day 65.7616 kg/day Fuel consumption per annum 19.72848 TPA Cost of fuel 31 Rs./kg Measured Data 40 °C Ambient air temperature: (WBT) 38 °C Material Temperature at feeding 40 °C Average Or supply air for combustion 40 °C Average Oxygen level 6.1 % Average CO level 9225 ppm Exit flue gas temperature 1050 °C Average surface temperature -front & back 200 °C Average surface temperature -front & back 200 °C Average surface temperature - Top 200 °C Surface area urface temperature - Top 200 °C Surface area - front & back 0.39903064 m² Surface area - front & back 0.37999924 m² Surface Area - Top	Ash content	0.35	% by mass
Fuel consumption per hour Fuel consumption per day Fuel consumption per day Fuel consumption per day Fuel consumption per annum Cost of fuel Measured Data Ambient air temperature: (DBT) Ambient air temperature at feeding Fuence on Supply air for combustion Average Oxygen level Average Oxygen level Average surface temperature - Tront & back Average surface temperature - Tront & back Average surface temperature - Tront & back Average surface temperature - Top Temperature at Discharge opening Surface area - front & back Surface Area - Top Surface Area - Top Surface Area - Top O.02725801 Area - Olscharge opening O.02725801 Area - Charge opening Area - Charge opening Area - Charge opening Surface Area - Top Surface Ar	Gross calorific value	10880	kcal/kg.
Fuel consumption per day Fuel consumption per day Fuel consumption per annum 19.72848 TPA Cost of fuel 31 Rs./kg Measured Data Ambient air temperature: (DBT) Ambient air temperature: (WBT) 38 °C Material Temperature at feeding 40 °C Average Oxygen level Average CO level Exit flue gas temperature - front & back Average surface temperature - front & back Average surface temperature - Top Cayreage surface temperature - Top Cayreage surface temperature - Top Cayreage act opening Average opening Average opening Average act - front & back Average surface temperature - Top Cayreage surface temperature - Top C	Bulk Density	920	kg/m ³
Fuel consumption per annum Cost of fuel Measured Data Ambient air temperature: (DBT) Ambient air temperature: (WBT) Material Temperature at feeding Average Oxygen level Exit flue gas temperature - main body Average surface temperature - Top Average surface temperature - Top Costrace area - main body Surface area - front & back Surface Area - Top Area - Charge opening Area - Charge opening Area - Charge opening Aterial Teeding Rate Asea of C Material Teeding Rate Appecific heat of steel Specific heat of steel Specific heat of steal Specific heat of steal Enthalpy of steam at flue gas temperature 40 Co Co Average Surface 31 Average Surface 40 Co Co Co Co Co Co Co Co Co C	Fuel consumption per hour	9.394514286	kg/hr
Cost of fuel 31 Rs./kg Measured Data Ambient air temperature: (DBT) 40 °C Ambient air temperature: (WBT) 38 °C Material Temperature at feeding 40 °C Temp. of supply air for combustion 40 °C Average Oxygen level 6.1 % Average CO level 9225 ppm Exit flue gas temperature 1050 °C Average surface temperature -main body 200 °C Average surface temperature -front & back 200 °C Surface area a main body 0.80903064 m² Surface area - front & back 0.399225728 m² Surface area - front & back 0.3999924 m² Area - Discharge opening 0.02725801 m² Area - Charge op	Fuel consumption per day	65.7616	kg/day
Measured Data Ambient air temperature: (WBT) 40 °C Ambient air temperature: (WBT) 38 °C Ambient air temperature: (WBT) 38 °C Material Temperature at feeding 40 °C Measured Data 40 °C Measured Data 40 °C Measured Colevel 9225 ppm Exit flue gas temperature 1050 °C Average surface temperature - main body 200 °C Average surface temperature - front & back 200 °C Average surface temperature - Top 200 °C Average surface temperature - Top 200 °C Temperature at Discharge opening 1090 °C Temperature at Charge opening 40 °C Surface area - main body 0.80903064 m² Surface Area - Top 0.37999924 m² Surface Area - Top 0.37999924 m² Area - Discharge opening 0.0225806 m² Material temperature at furnace exit 1090 °C	Fuel consumption per annum	19.72848	TPA
Ambient air temperature : (WBT) 38 °C Ambient air temperature : (WBT) 38 °C Material Temperature at feeding 40 °C Temp. of supply air for combustion 40 °C Average Oxygen level 6.1 % Average CO level 9225 ppm Exit flue gas temperature 1050 °C Average surface temperature -main body 200 °C Average surface temperature -front & back 200 °C Average surface temperature - Top 200 °C Temperature at Discharge opening 1090 °C Temperature at Charge opening 40 °C Surface area - main body 0.80903064 m² Surface area - front & back 0.39225728 m² Surface area - Top 0.37999924 m² Area - Discharge opening 0.02725806 m² Area - Charge opening 0.0225806 m² Material Feeding Rate 89.88571429 kg/hr Material Feeding Rate 89.88571429 kg/hr Material Feeding Rate 629.2 kg/day </td <td>Cost of fuel</td> <td>31</td> <td>Rs./kg</td>	Cost of fuel	31	Rs./kg
Ambient air temperature : (WBT) Material Temperature at feeding Temp. of supply air for combustion Average Oxygen level Average CO level Exit flue gas temperature Average surface temperature - main body Average surface temperature - Top Average surface temperature - Top Temperature at Discharge opening Surface area - main body Surface area - front & back Surface area - front & back Area - Discharge opening Area - Charge opening Area - Charge opening Area - Charge opening Area - Charge opening Atterial temperature at furnace exit Material Feeding Rate Specific heat of water Specific heat of steel Specific heat of water vapour at flue gas tempe Enthalpy of water at supply air temperature 40 C C C C C C C C C C C C C	Measured Data		
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Temp. of supply air for combustion Average Oxygen level Average CO level Page 5 Average CO level Page 5 Average Surface temperature Average surface temperature -main body Average surface temperature -front & back Average surface temperature - Top Average surface temperature - Top Page 5 Average surface temperature - Top Average Surface Area - Top Average opening Average Colevel Average Surface Area - Top Area - Discharge opening Average Surface Area - Top Area - Charge opening Average Surface Area - Top Average Sur	Ambient air temperature : (WBT)	38	°C
Average Oxygen level 6.1 % Average CO level 9225 ppm Exit flue gas temperature 1050 °C Average surface temperature -main body 200 °C Average surface temperature -front & back 200 °C Average surface temperature - Top 200 °C Temperature at Discharge opening 1090 °C Temperature at Charge opening 40 °C Surface area - main body 0.80903064 m² Surface area - front & back 0.39225728 m² Surface Area - Top 0.3799924 m² Area - Discharge opening 0.02725801 m² Area - Charge opening 0.02725801 m² Aterial temperature at furnace exit 1090 °C Material temperature at furnace exit 1090 °C Material Feeding Rate 89.88571429 kg/hr Material Feeding Rate 629.2 kg/day Standard Data Specific heat of water 1 kcal/kg °C Specific Heat of coal 0.25 kcal/kg °C Specific heat of water 0.52 kcal/kg °C Specific heat of water at supply air temperature 639.9 kcal/kg Specific Heat of flue gas 0.331949568 kcal/kg °C	Material Temperature at feeding	40	°C
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Average surface temperature -main body Average surface temperature -front & back 200 C Average surface temperature - Top 200 C Temperature at Discharge opening 1090 C Surface area - main body Surface area - front & back 0.39925728 M² Surface area - Top 1090 C Surface area - Top 30,3799924 Area - Discharge opening Area - Charge opening Material temperature at furnace exit 1090 C Material Feeding Rate 89.88571429 Kg/hr Material Feeding Rate Specific heat of water Specific Heat of steel Specific heat of saver Specific heat of water vapour at flue gas tempe Enthalpy of steam at flue gas Specific Heat of flue gas Specific Heat of flue gas C Specific Heat of flue gas C Specific Heat of flue gas Specific Heat of flue gas C Specific Heat of flue gas C Specific Heat of flue gas	Average CO level	9225	ppm
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Enthalpy of water at supply air temperature 40 kcal/kg Specific Heat of flue gas 0.331949568 kcal/kg °C		0.52	kcal/kg °C
Specific Heat of flue gas 0.331949568 kcal/kg °C	Enthalpy of steam at flue gas temperature		kcal/kg
		40	kcal/kg
Moisture content of supply air 0.019 kg/kg of air			3
	Moisture content of supply air	0.0	19 kg/kg of air

		Results Sheet
Efficiency Calculation of Furnace		
Name of unit	Rajasthan Tools	
No. of Furnaces	1	
Type of furnace	Plier	
Application of furnace	160 mm	
Raw material under process	EN8	
Production Capacity	0.6292	TPD
Material feeding rate	89.88571429	kg/hr
Fuel Consumption rate	9.39	kg/hr
Specific heat of the material	0.12	kcal/kg °C
Material temperature at furnace entry	40	°C
Material temperature at furnace exit	1090	°C
Furnace efficiency by direct method	11.1	%
Furnace efficiency by heat loss method		
Stoichiometric air required for combustion	12.913	kg/kg of fuel
Theoretical max. CO ₂	17.44	%
Measured O ₂ in flue gas	6.1	%
Measured CO in flue gas	9225	ppm
Excess air used for combustion	40.94	%
Corresponding CO ₂	12.37	%
Total air used for combustion	18.20	kg/kg of fuel
Heat loss due to dry flue gas	60.35	%
Heat loss due to moisture in fuel	0.019	%
Heat loss due to Hydrogen in fuel	7.24	%
Heat loss due to moisture in air	1.67	%
Heat loss due to CO formation	3.23	%
Heat loss due to radiation & openings	5.49	%
Heat loss in scale generation	0.0	%
Heat content in the material	11.08	%
Unaccounted loss	10.92	%

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